

Industrial applications of large-scale and distributed optimization

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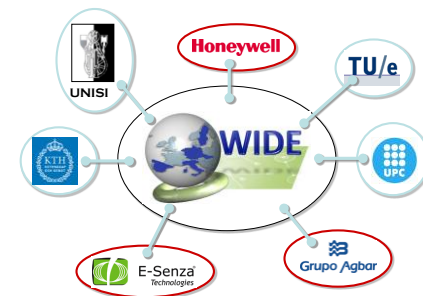
²) Honeywell
Automation and Control Solutions
ACS Global Laboratory Prague



Honeywell



- **Large-scale distributed networked systems**
- **Water distribution network optimization**
 - Hierarchy
 - Control objectives & problem formulation
 - DMPC for transport layer
- **Application with AGBAR Barcelona network**
 - Benefit evaluation tool
 - Real-time closed loop DMPC demo (EU FP7 WIDE project)
 - Conclusions





Typical large-scale networked systems

- Water / gas distribution networks
- River cascade dams control
- Electricity distribution – current smart grid solutions are variations on presented methods
- Logistic problems (integer optimization)

Control solution

- Suitable for Model Predictive Control (MPC)
- Translates to QP for linear dynamic process models
- Computation complexity grows quickly with problem size



Water Network Control Center
AGBAR Barcelona



Water treatment layer

- Mechanical / chemical / biological water treatment
 - Different water quality
 - Different processing cost

Water transport layer

- Transport to storage tanks (water towers)
- Control of pumping stations and valves
 - Pumping cost
 - Periodic demand
 - Limited storage capacity

Water distribution layer

- Distribution to end users
 - Control of pressure reducing valves and booster pumps
 - Major losses occur here

Sewage water collection and treatment

- Similar hierarchy



Water treatment layer

- Continuous process control methods
 - Large time constants
 - Large storage capacity
 - Cumulative constraints on availability

Water transport layer

- Networked control problem
 - Typical sampling interval 1 hour
 - Control / optimization horizon up to 1 week
(need to capture periodic demand, varying electricity tariffs, varying production costs, impact on water quality (storage, ageing))
- Current solution
 - Heuristic control law with operator interventions
- Next generation solution
 - Large-scale spatially distributed control & optimization problem
 - Can be solved by distributed MPC
 - Complex optimization criteria embedded

} ... this talk

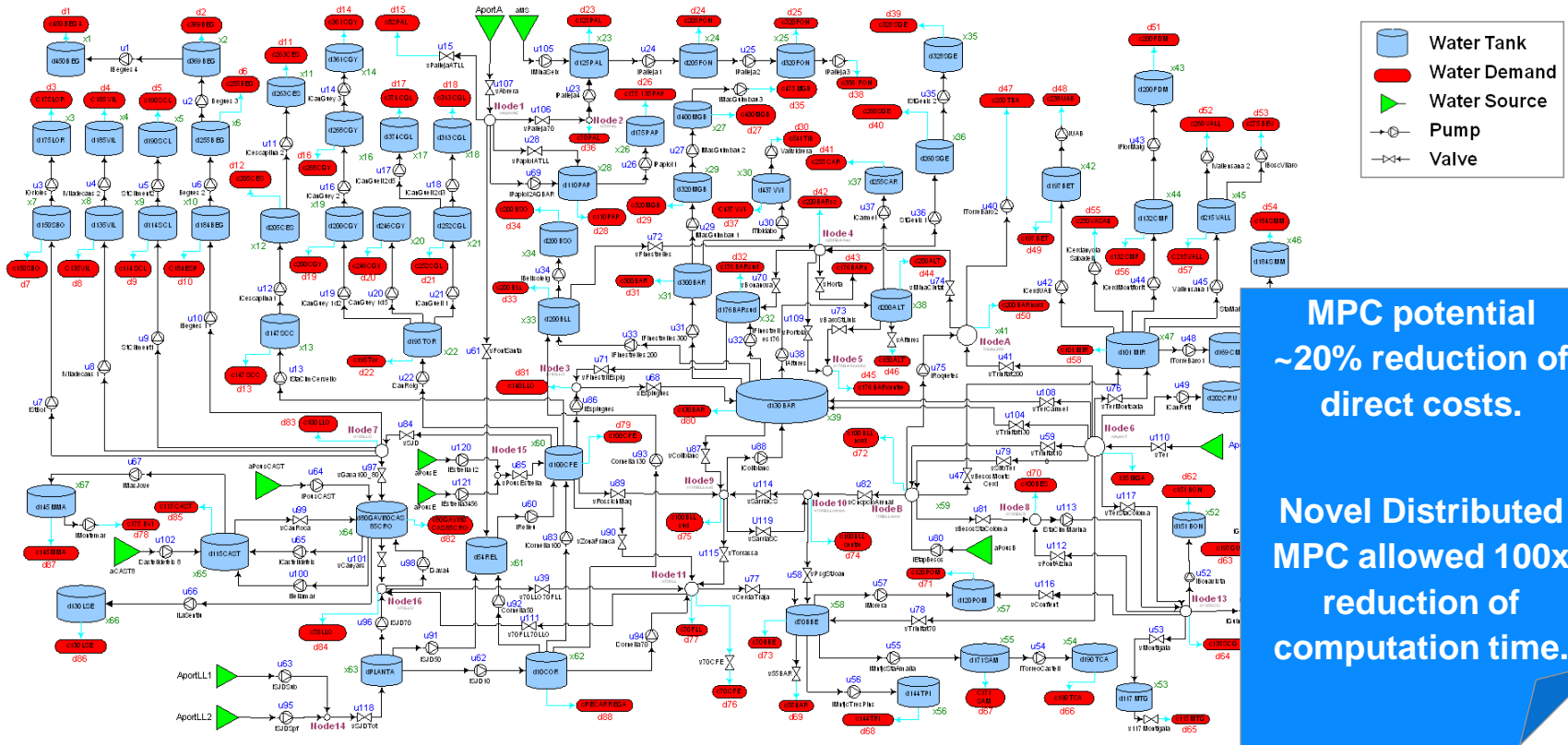


Water distribution layer

- **Network control problem**
 - Sampling period < 1 second (pressure control = stiff problem)
- **Current solution**
 - PLCs /mechanical PRVs with several preprogrammed pressure levels (day/night) in the distribution network feeding points (Pressure Reducing Valves)
- **Next generation solution**
 - **Active pressure zone control**
 - ◆ Closed loop, multivariable solution
 - ◆ Flow / pressure sensor network
 - **Network monitoring and data reconciliation**
 - ◆ Introduction of smart sensors
 - **Leaking detection and failure recovery to minimize water losses**
 - ◆ Detect abrupt changes (bursts) as well as background losses (drift)
 - ◆ Bottom-up approach - pressure zone modeling
 - ◆ Top-down approach - balancing individual metered areas



Barcelona Water Distribution Network



**MPC potential
~20% reduction of
direct costs.**

**Novel Distributed
MPC allowed 100x
reduction of
computation time.**

Network Size

- 70 tanks
- 110 pumps/valves
- 80 demands (disturbances)
- 9 water sources
- 1 hour sampling time
- 24-48 step prediction
- 5000 - 10000 variables



CONTROL OBJECTIVES

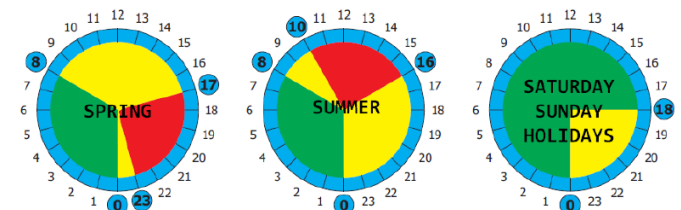
- Satisfaction of water demand (avoid exceeding tank safety limits – range control)
- Minimization of operation costs
- Manipulated variables
 - pump flows
 - valve flows
 - water sources production



Tank and pumping station

OPTIMIZATION POTENTIAL

- Time varying electricity price during the day
- Different costs of water sources (rivers, wells, etc.)
- Multiple possible routes from sources to consumers
- Operation costs can be mainly reduced
 - Using network storage capacity by pumping in the periods of cheap electricity
 - Optimal routing of water from sources to tanks and blending



Electricity price patters during different days

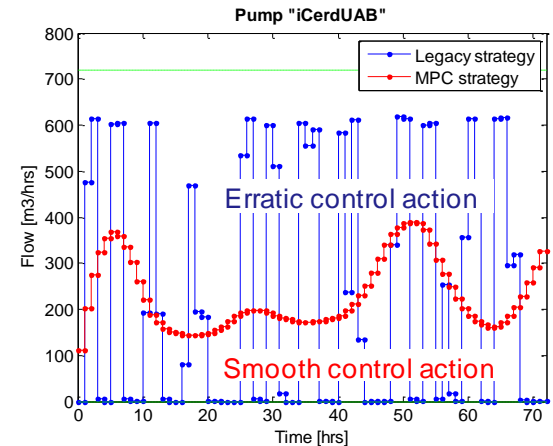


Indirect costs

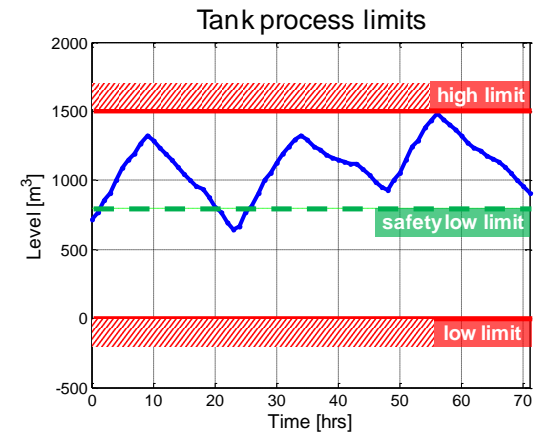
- Reduction of large set point changes for pumps, valves and water sources:
 - Reducing pressure surges (leakage prevention)
 - Reducing equipment tear & wear
- Water ageing – long water storage degrades its quality and requires additional chlorination

Constraints

- Hard constraints
 - Actuator limits & rate-of-change limits
 - Pumps, valves and water sources
- Soft constraints
 - tanks minimum safety limits
- Constraints are time variable (maintenance, failures)



Smooth vs. erratic pump control action



Soft safety limits

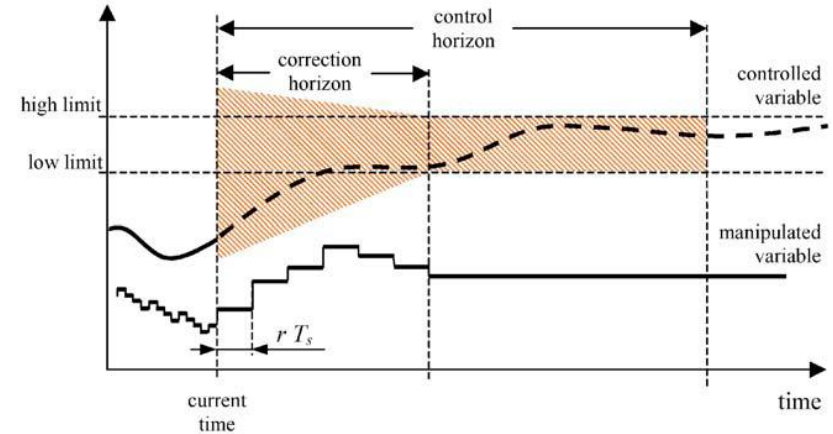


Basic MPC problem

- **K-step ahead prediction horizon**
- **Reference tracking**
- **Hard constraints on MV, ΔMV**
(all constraints can be time varying)

$$\min_{u_1, \dots, u_K} \sum_{k=1}^K (y_k - r_k)^T Q_k (y_k - r_k) + \Delta u_k^T R_k \Delta u_k$$

$$u_L \leq u_k \leq u_H; \quad \Delta u_L \leq \Delta u_{t+k} \leq \Delta u_H$$



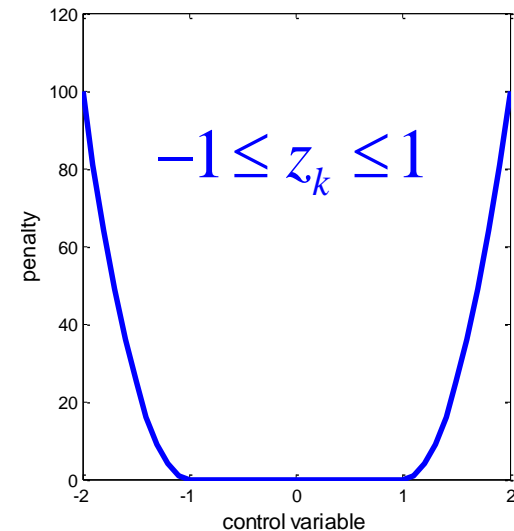
Range control concept

- **Soft constraints on CVs**
- **Auxiliary variable z_k**
- **Additional degree of freedom for optimization**

$$\min_{\substack{u_1, \dots, u_K \\ z_1, \dots, z_K}} \sum_{k=1}^K (y_k - z_k)^T Q_k (y_k - z_k) + \Delta u_k^T R_k \Delta u_k$$

$$u_L \leq u_k \leq u_H; \quad \Delta u_L \leq \Delta u_{t+k} \leq \Delta u_H$$

$$y_L \leq z_k \leq y_H$$





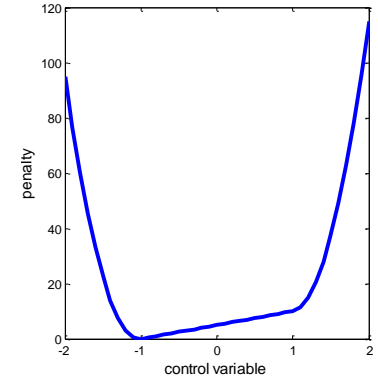
Additional “economic” cost terms (linear)

- Pumping cost – time varying electricity tarif
- Water sources cost
- Water aging / storage cost

$$\min_{\substack{u_1, \dots, u_K \\ z_1, \dots, z_K}} \sum_{k=1}^K (y_k - z_k)^T Q_k (y_k - z_k) + \Delta u_k^T R_k \Delta u_k + C_k^P u_k + C_k^W u_k + C_k^S (y_k - y_L)$$

$$u_L \leq u_k \leq u_H; \quad \Delta u_L \leq \Delta u_k \leq \Delta u_H$$

$$y_L \leq z_k \leq y_H$$



Optimization problem

- Use current state, control sequence u_1, \dots, u_K and predicted disturbance sequence d_1, \dots, d_K to calculate controlled variables y_1, \dots, y_K
- Substitute into criterion
- Resulting problem
 - (Large scale) quadratic programming
 - Can be solved in distributed way

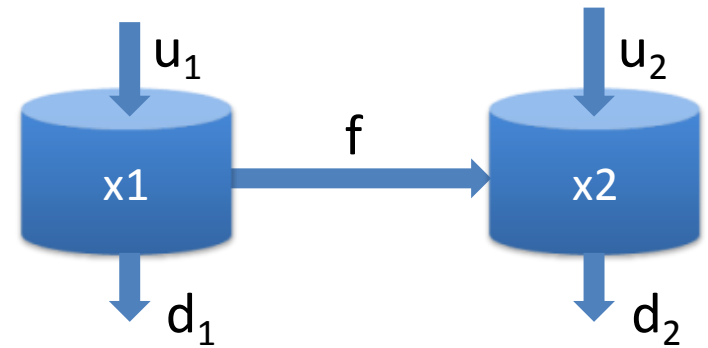


Approach: dual decomposition

Distributed MPC problem

$$\min_{u_1, u_2, f} J(u_1, u_2, f) = \min_{u_1, f} J_1(u_1, f) + \min_{u_2, f} J_2(u_2, f)$$

$$\underline{u}_i \leq u_i \leq \bar{u}_i, \underline{f} \leq f \leq \bar{f}, \underline{x}_i \leq x_i \leq \bar{x}_i$$



Duplicating complicating variable f

$$\min_{u_1, u_2, f_1, f_2} J_1(u_1, f_1) + J_2(u_2, f_2) \quad \text{s.t.} \quad f_1 = f_2$$

Lagrangian

$$L(u_1, u_2, f_1, f_2, \lambda) = J_1(u_1, f_1) + J_2(u_2, f_2) + \lambda^T (f_1 - f_2)$$

Dual function

$$g(\lambda) = \min_{u_1, u_2, f_1, f_2} L(u_1, u_2, f_1, f_2, \lambda)$$

$$= g_1(\lambda) + g_2(\lambda)$$

can be separated

$$g_1(\lambda) = \min_{u_1, f_1} J_1(u_1, f_1) + \lambda^T f_1$$

$$g_2(\lambda) = \min_{u_2, f_2} J_2(u_2, f_2) - \lambda^T f_2$$

Optimal solution (saddle point theorem) – “shadow price”

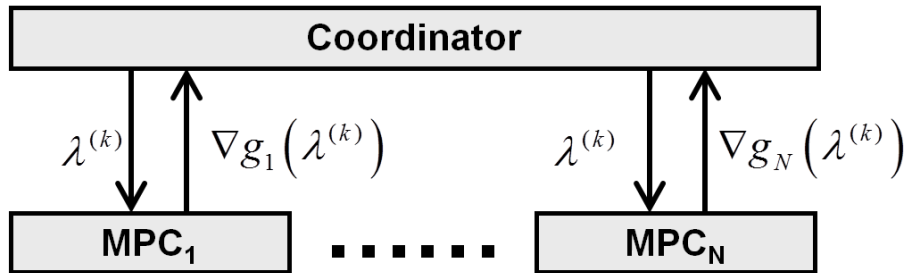
$$\lambda^* = \arg \max_{\lambda} g(\lambda)$$



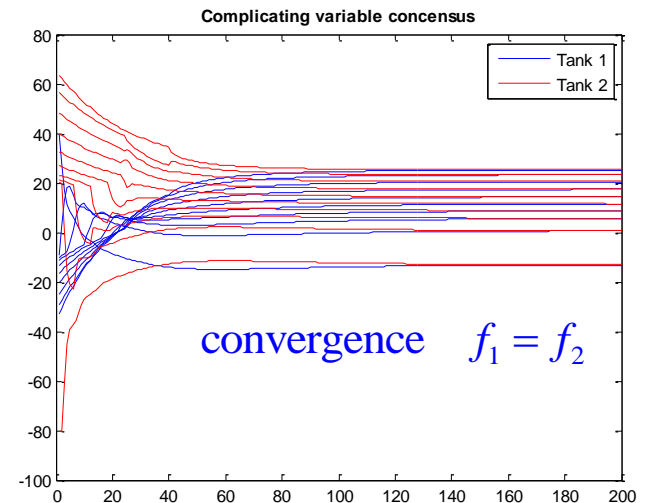
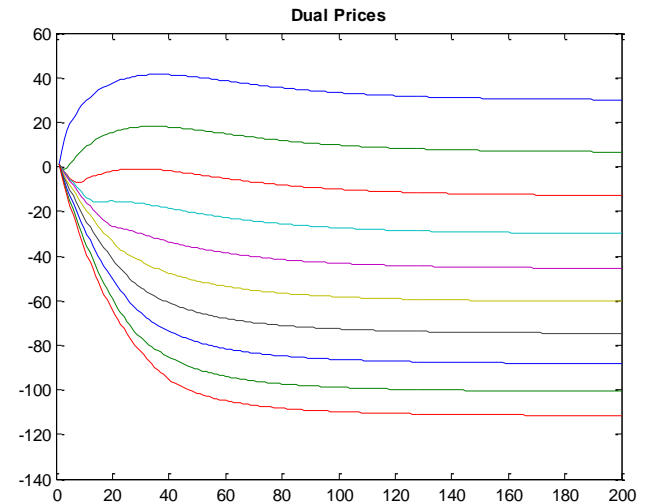
Two Tanks Example

Maximizing dual function (grad. method)

$$\lambda^{(k+1)} = \lambda^{(k)} + \alpha^{(k)} \left(\frac{\partial g_1}{\partial \lambda} + \frac{\partial g_2}{\partial \lambda} \right) \Big|_k \quad \frac{\partial g_1}{\partial \lambda} \Big|_k = f_1^{(k)*} \quad \frac{\partial g_2}{\partial \lambda} \Big|_k = -f_2^{(k)*}$$

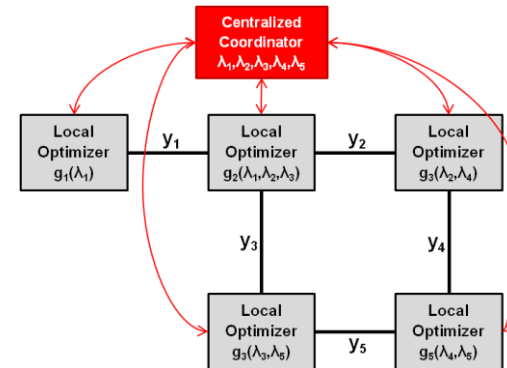
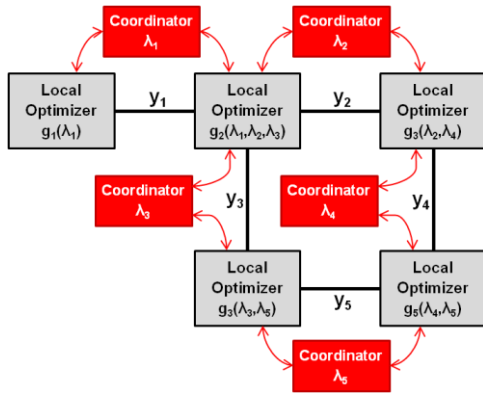


- MPC control horizon $K = 20$
- Simple gradient method
 - High number of iteration (~ 200)
- Large improvement
 - Nesterov accelerated gradient method
 - Still too many iterations for Barcelona sized network





$$\max_{\lambda} g(\lambda), \quad g(\lambda) = \sum_i g_i(\lambda)$$



LOCAL (distributed)

- Gradient method exploiting problem structure (components computed locally)

$$\frac{\partial g}{\partial \lambda_3} = \frac{\partial g_2}{\partial \lambda_3} + \frac{\partial g_3}{\partial \lambda_3}$$

- Computing derivatives requires to solve local sub-problems for given λ

$$\left. \frac{\partial g_i}{\partial \lambda} \right|_k = f_i^{(k)*}$$

CENTRALIZED

- Captures the multivariable problem (interactions between λ_i)
- Significantly improved convergence
 - Newton type methods
 - Quasi-Newton type methods
 - Structure: local optimizers provide components of Hessian
- Requires centralized communication
- Coordinator computation complexity



Parametric price coordination

- For LQ problem, local dual functions are **piece-wise quadratic on polytopic regions**
- Local controllers provide quadratic parameters valid in current polytopic region

$$g_i(\lambda) = \lambda^T A_i \lambda + b_i^T \lambda + c_i \quad s.t. \quad \lambda \in P_i$$

- Optimal local solution is affine in current region

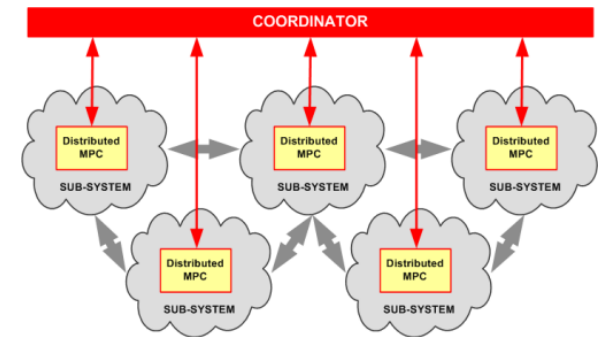
$$\begin{bmatrix} x_i^*(\lambda) \\ f_i^*(\lambda) \end{bmatrix} = F_i \lambda + g_i \quad \text{for} \quad H_i \lambda \leq k_i$$

- Optimal dual solution can be obtained in single step if feasible

$$\nabla^2 g(\lambda_k) v_k = -\nabla g(\lambda_k) \quad \text{such that} \quad \lambda_k + v_k \in \bigcap P_i$$

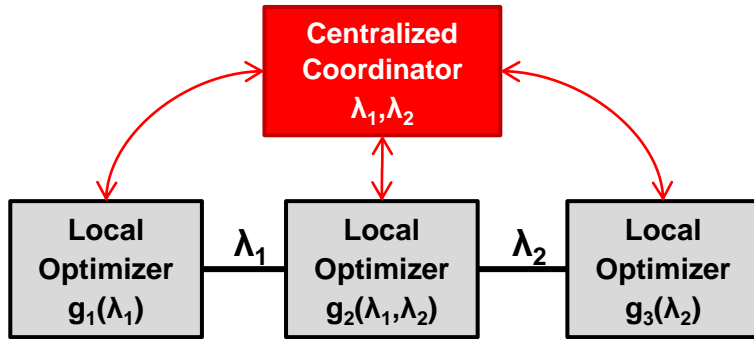
otherwise use damped Levenberg-Marquardt

$$(\varepsilon I + \nabla^2 g(\lambda_k)) v_k = -\nabla g(\lambda_k)$$





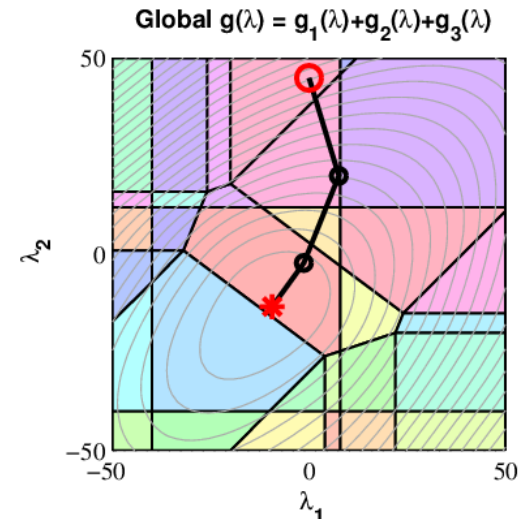
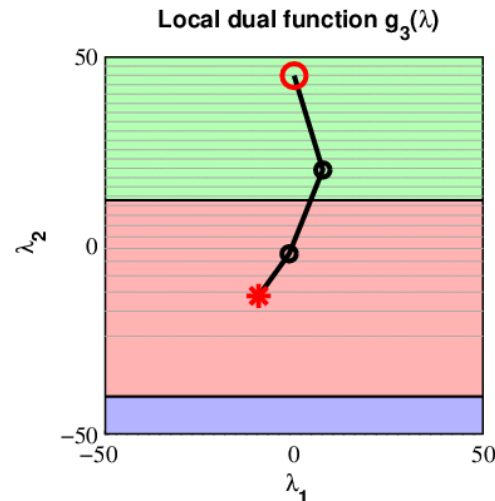
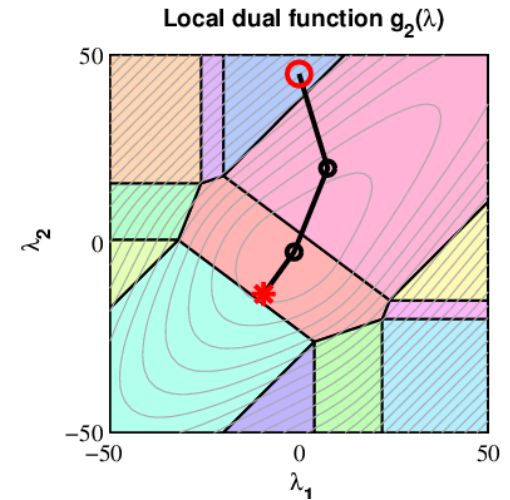
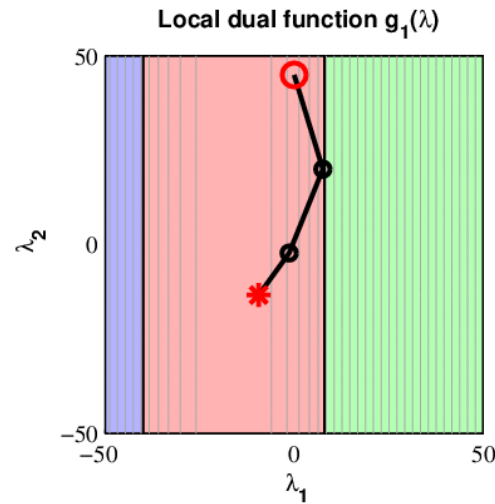
Parametric coordination – example



$$g(\lambda) = g_1(\lambda) + g_2(\lambda) + g_3(\lambda)$$

$$\max_{\lambda} g(\lambda)$$

- Illustration of the local dual functions composition
- Coordinator can use this fact to improve convergence and reduce communication load





Parametric coordination – example

- Local controllers return quadratic parameters and their polytopic validity region around given price vector (local solution)

$$g_i(\lambda) = \lambda^T A_i \lambda + b_i^T \lambda + c_i$$

such that $\lambda \in P_i$

i.e. $H_i \lambda \leq k_i$

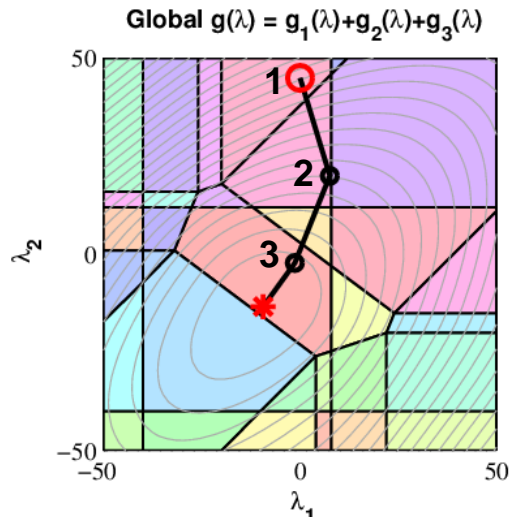
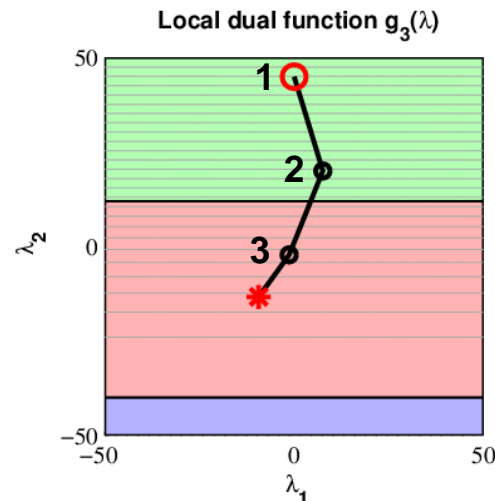
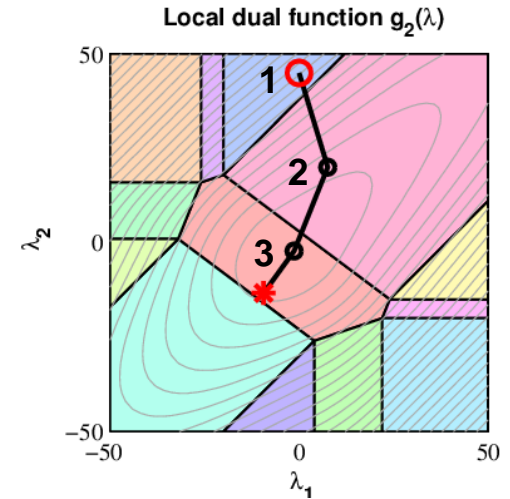
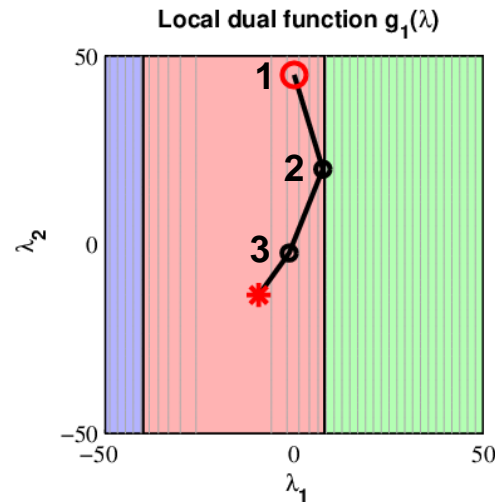
- Local solutions are kept between iterations

- Recalculation required only if invalidated by shadow price update

$$\lambda^{(k+1)} \notin P_i$$

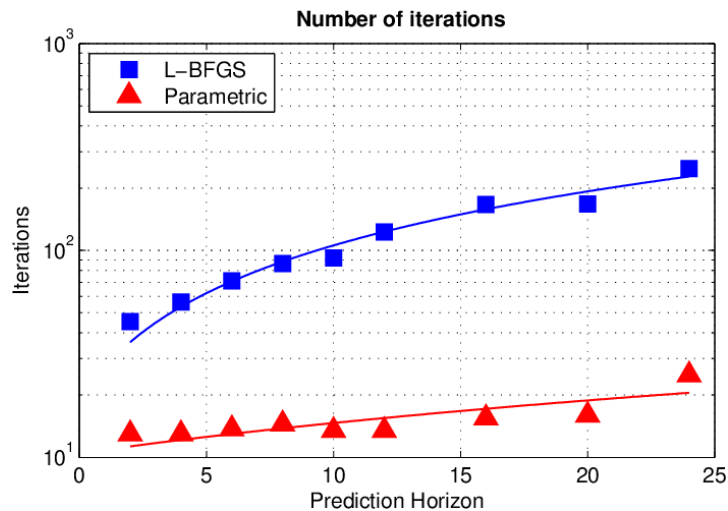
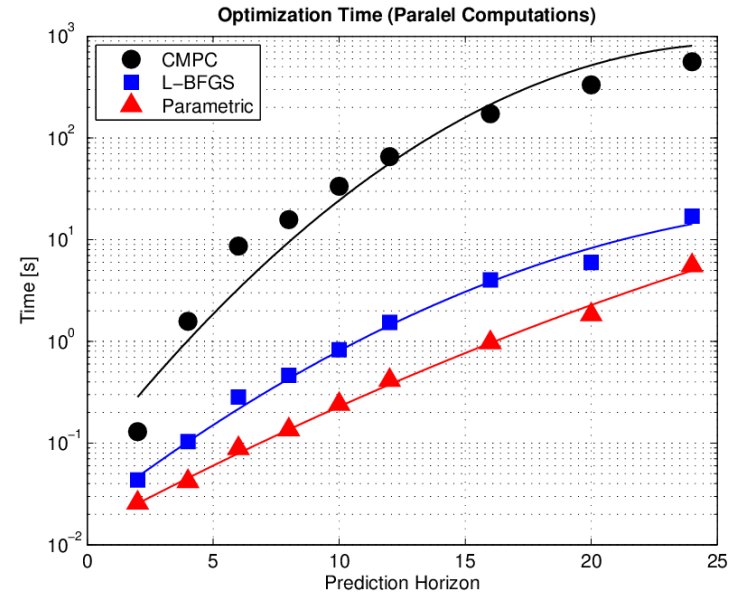
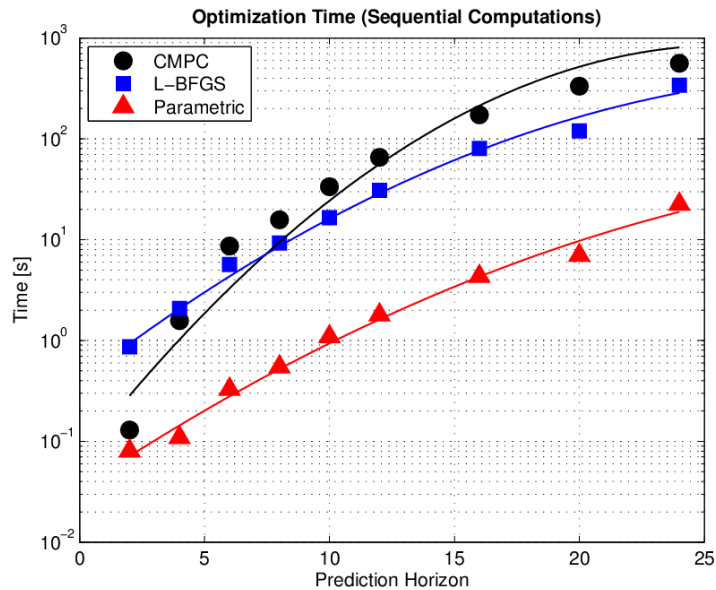
- Coordination process

- Newton method with Levenberg-Marquardt damping
- Switching on region borders not efficient





DMPC Results on Barcelona Network



Summary

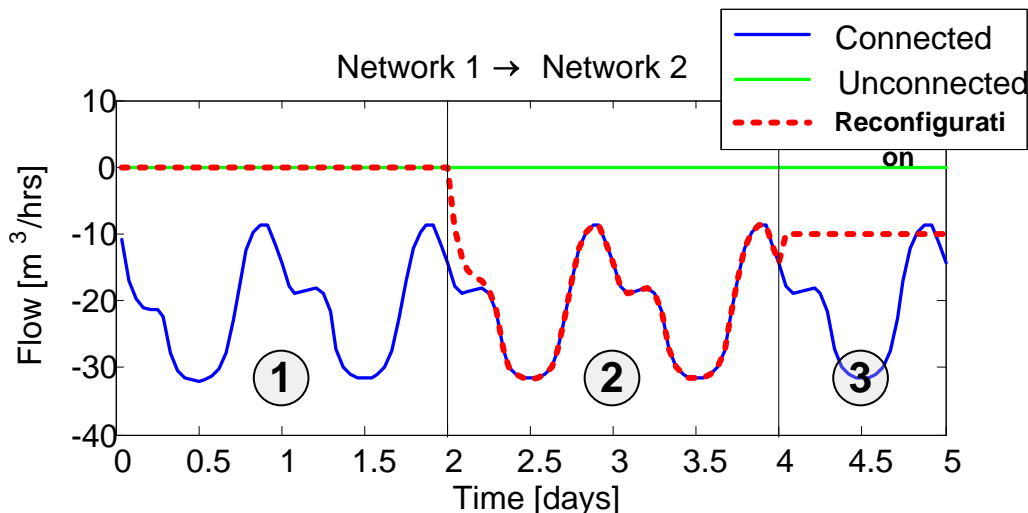
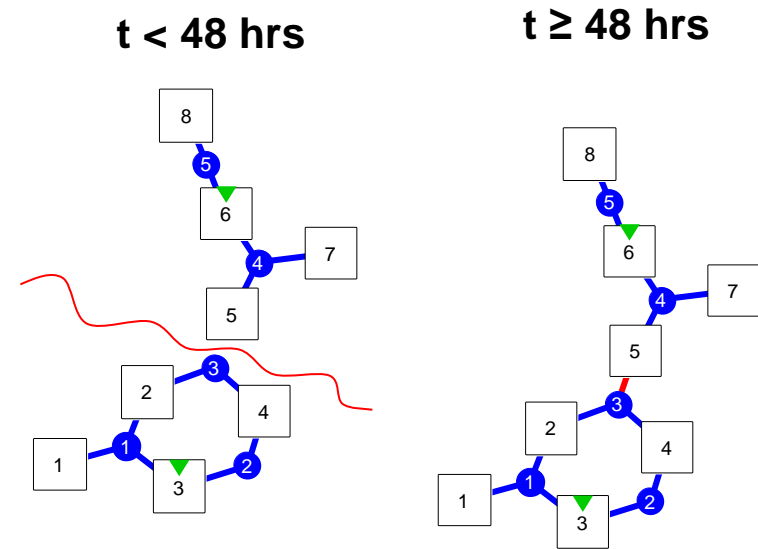
- ~10x reduction in a number of iterations (compared to Quasi-Newton L-BFGS)
- Only ~25% of local problems are recalculated in each iteration
- ~100x faster than centralized MPC
~10x faster than L-BFGS



DMPC Modularity (topology changes)

Decentralized control based on Dual Decomposition allows **simple changes in network configuration** without any global adjustments while preserving centralized MPC optimality:

- 1 $t < 48$ networks are unconnected
- 2 $t = 48$ networks are connected
- 3 $t \geq 96$ connecting pump is switched to MAN



Blue line – optimal control of connected networks on the whole interval

Green line – optimal control of unconnected networks on the whole interval

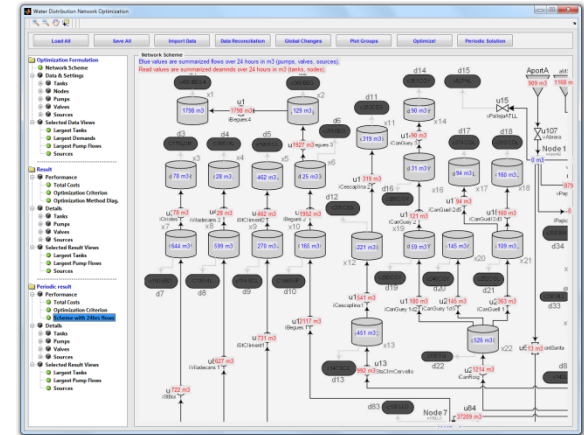


Implementation: Benefits Evaluation Tool

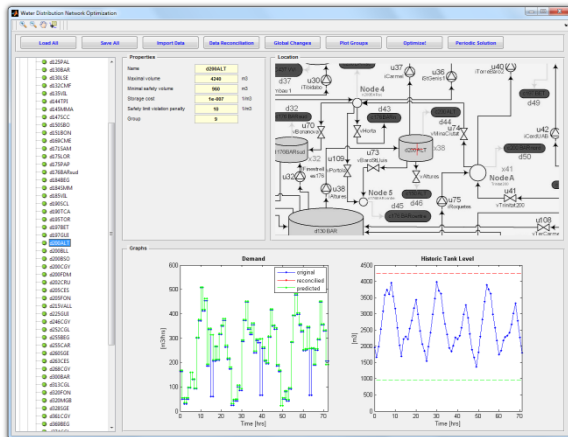
Honeywell

Off-line tool with GUI (in Matlab)

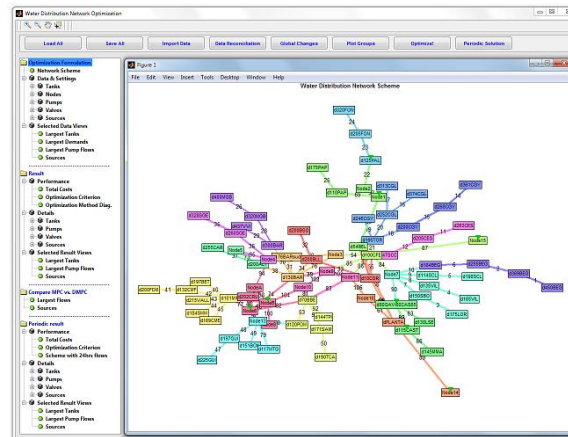
- Building water network topology
- Setting process limits and prices
- Importing historic data (with reconciliation)
- Performing optimization
- Comparing flow and tank level trajectories between historic data and MPC strategy
- Evaluating benefits (pumping and water costs)



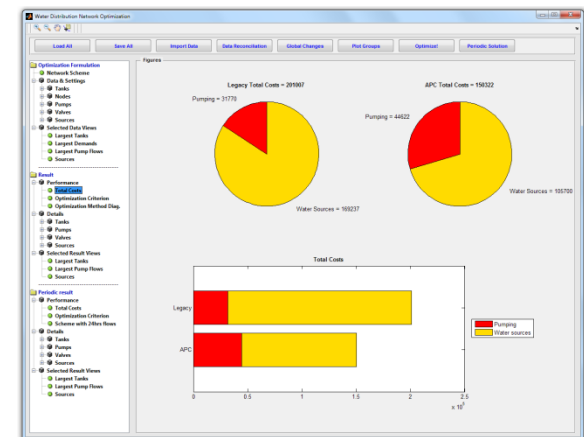
Network topology



Network object details view



Network separation to groups



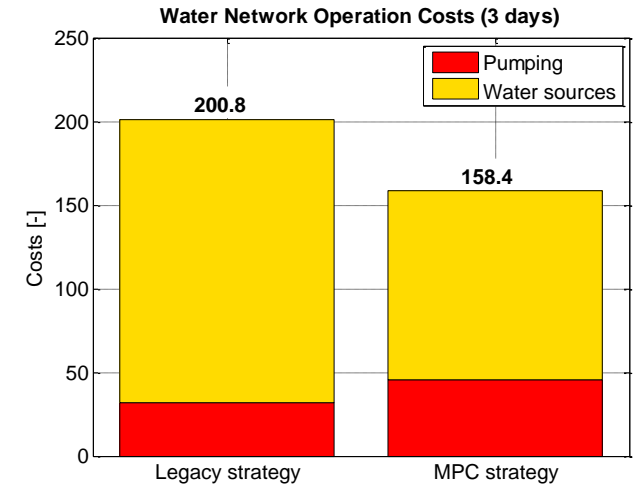
Costs evaluation



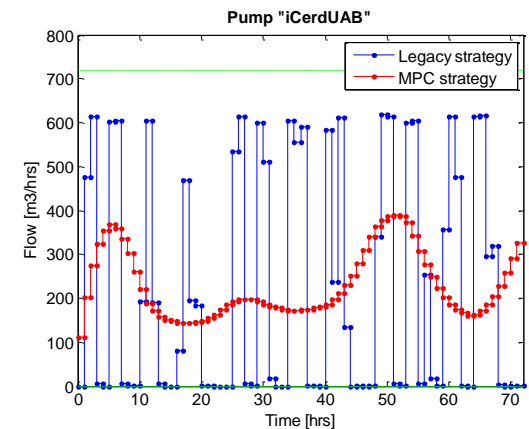
Based on historical data set

- ~20% direct cost savings
 - Increased pumping cost
 - Reduced cost of water treatment
 - Periodic operation enforced
- Indirect savings
 - smooth MV's operation / source loading
 - leakage prevention by small pressure surges
 - reduced equipment wear & tear

Operation costs comparison



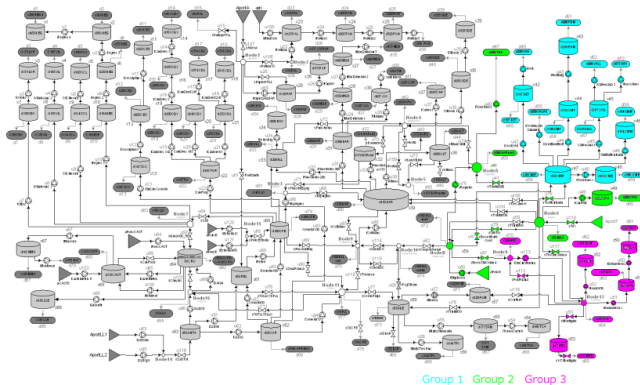
Indirect benefits (calm control actions)



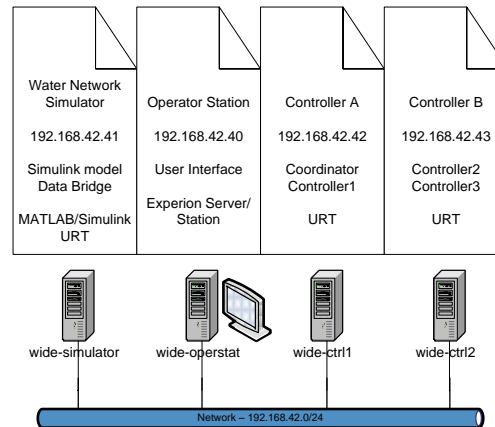


Implementation: Real-time DMPC Demo

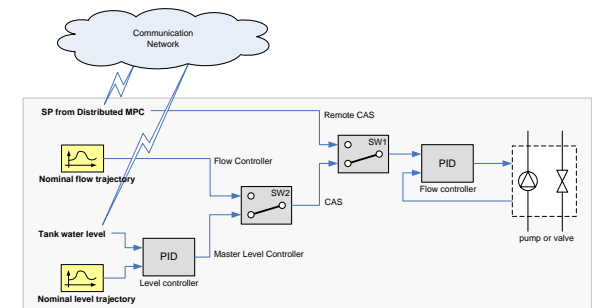
- **Complete control solution** on 3 selected areas of Barcelona Water Network
 - Algorithms implemented in C++ for **Honeywell Unified Real Time (URT) platform** – infrastructure for implementing advanced process control (power plants, chemical processes)
 - Design of basic control layer and backup control strategy (industrial Experion PIDs)
 - Operator panels (industrial Experion HMIweb)
- **Demonstrates project life cycle** - the ability of distributed MPC to replace legacy control in multiple steps for smooth transition between legacy and advanced control strategy
- Water network is simulated – hidden for control layer by standard OPC connectivity
- Areas controlled by 3 distributed MPC controllers



3 selected areas of Barcelona network

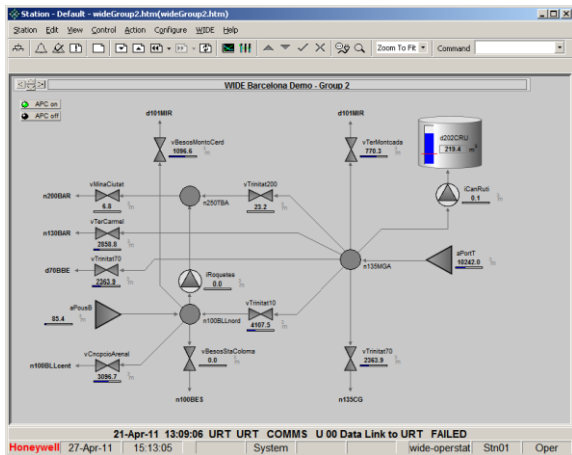


Control configuration on 4 computer: Flow controller with backup control

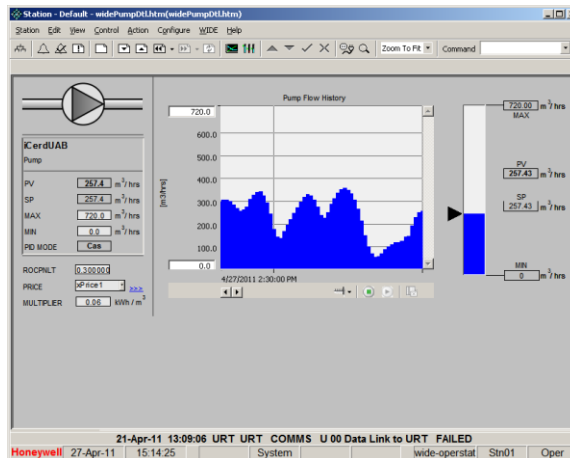




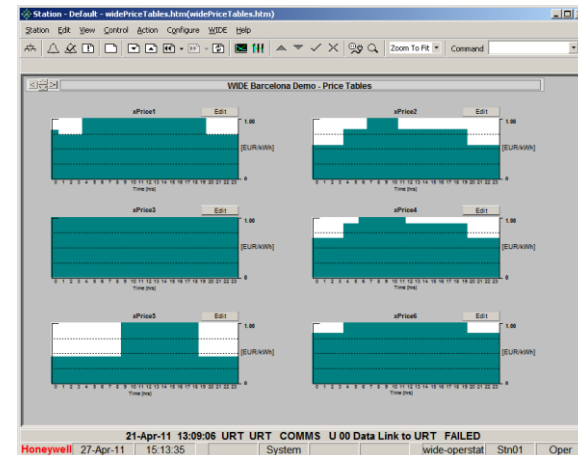
Implementation: Real-time DMPC Demo



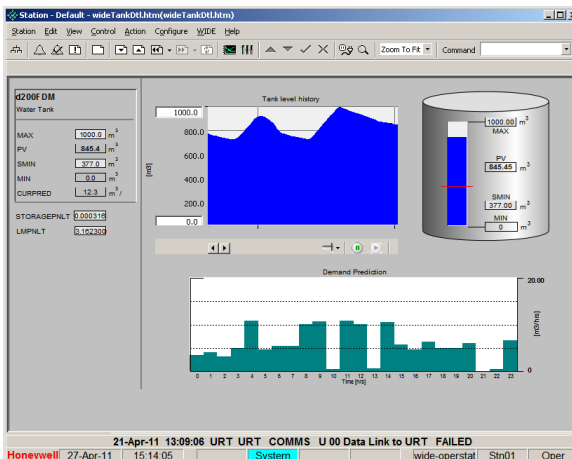
Network part detail



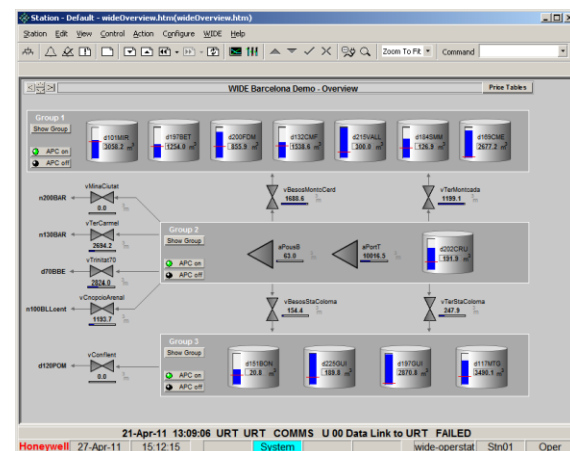
Pump details and history



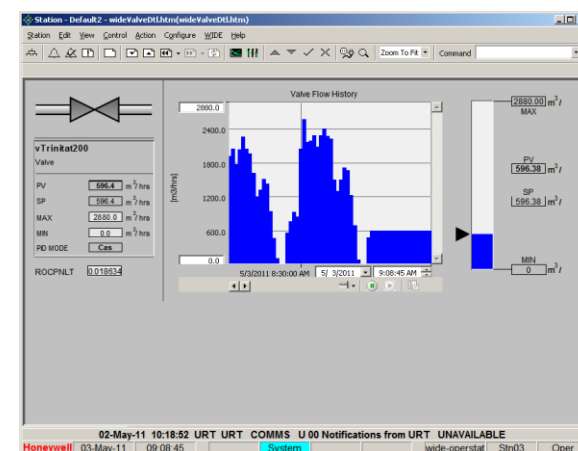
Electricity price patterns definitions



Tank details and history



Overview



Valve details and history



- **Distributed optimization is a strong framework for challenging size problems**
- **Distributed implementation of MPC is straightforward**
- **MPC-like sparse QP problems can be coordinated very efficiently**
- **Solution based on DMPC is mature for real applications**